

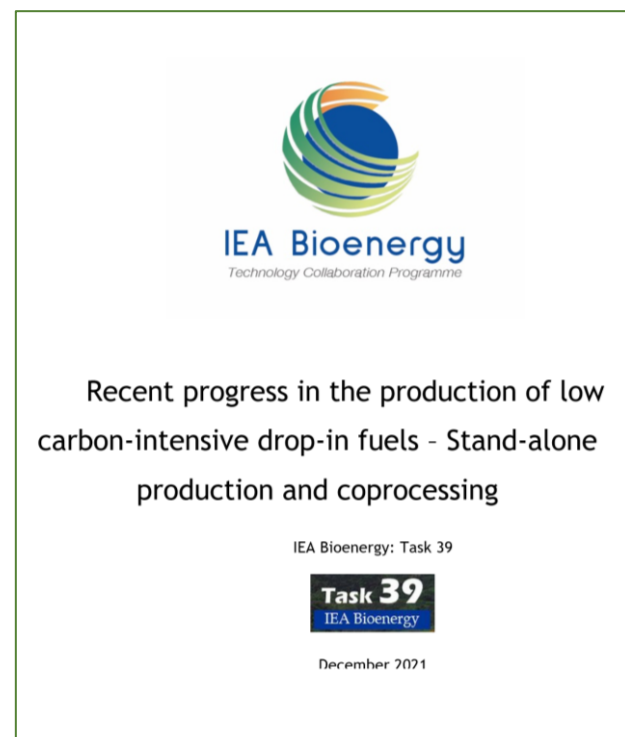
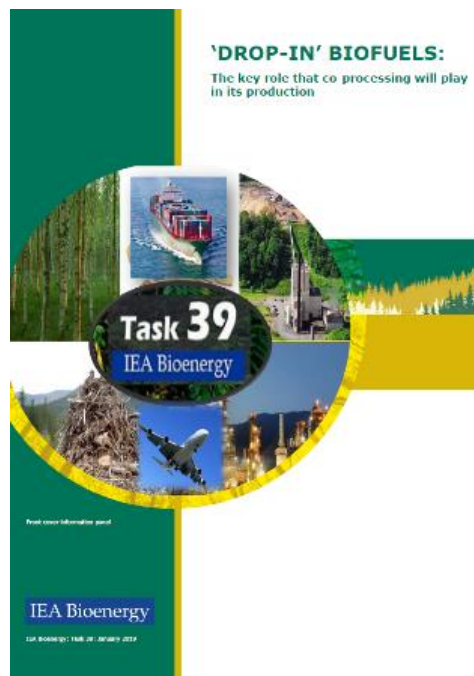
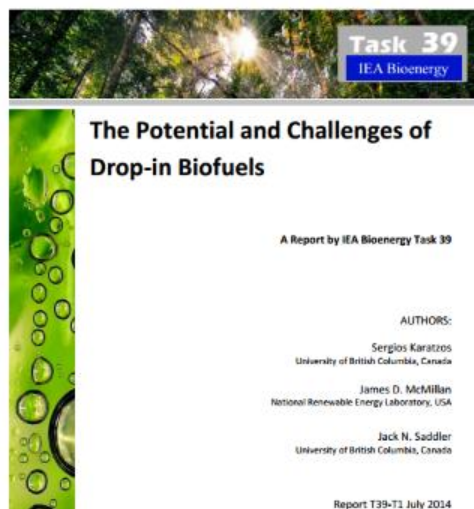
# Recent progress in the production of low carbon-intensive drop-in fuels - Stand-alone production and coprocessing

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*The IEA Bioenergy Technology Collaboration Programme (TCP) is organised under the auspices of the International Energy Agency (IEA) but is functionally and legally autonomous. Views, findings and publications of the IEA Bioenergy TCP do not necessarily represent the views or policies of the IEA Secretariat or its individual member countries.*

# Drop-in biofuels reports (2014, 2019 & 2021)



## Definition of “drop-in” biofuels

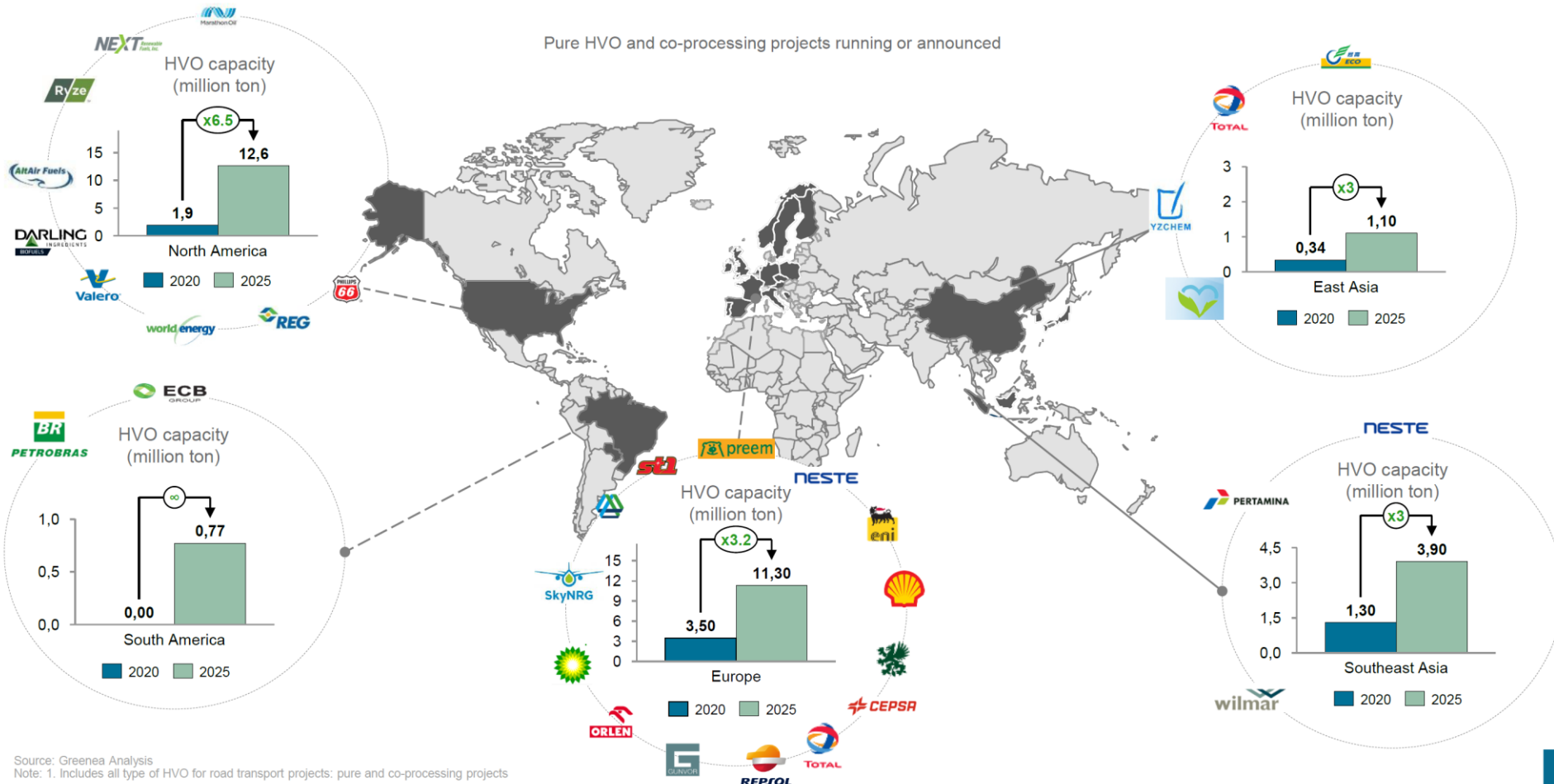
- Drop-in biofuels: are “liquid bio-hydrocarbons that are: **functionally equivalent** to petroleum fuels and **fully compatible with** existing petroleum infrastructure”

# Progress in drop-in biofuel production

- Stand-alone facilities
  - **New** construction (HVO/HEFA, Gasification/FT, Alcohol-to-jet, HTL, etc.)
  - **Repurposing** of old or disused refineries (HVO/HEFA)
  - Stand-alone facilities are prevalent for FOGs, many based on repurposing, e.g. World Energy, Neste, Phillips66, Marathon, etc.
  - Density of FOGs feedstocks allow large-scale facilities to achieve economies of scale
- Co-processing
  - Based on FOGs (fats, oils, and greases) - fully commercial
  - Bio-oil/Biocrude co-processing still being developed (limited volumes, technical challenges)

# Global HVO/HEFA expansion - will be limited by feedstock availability and cost

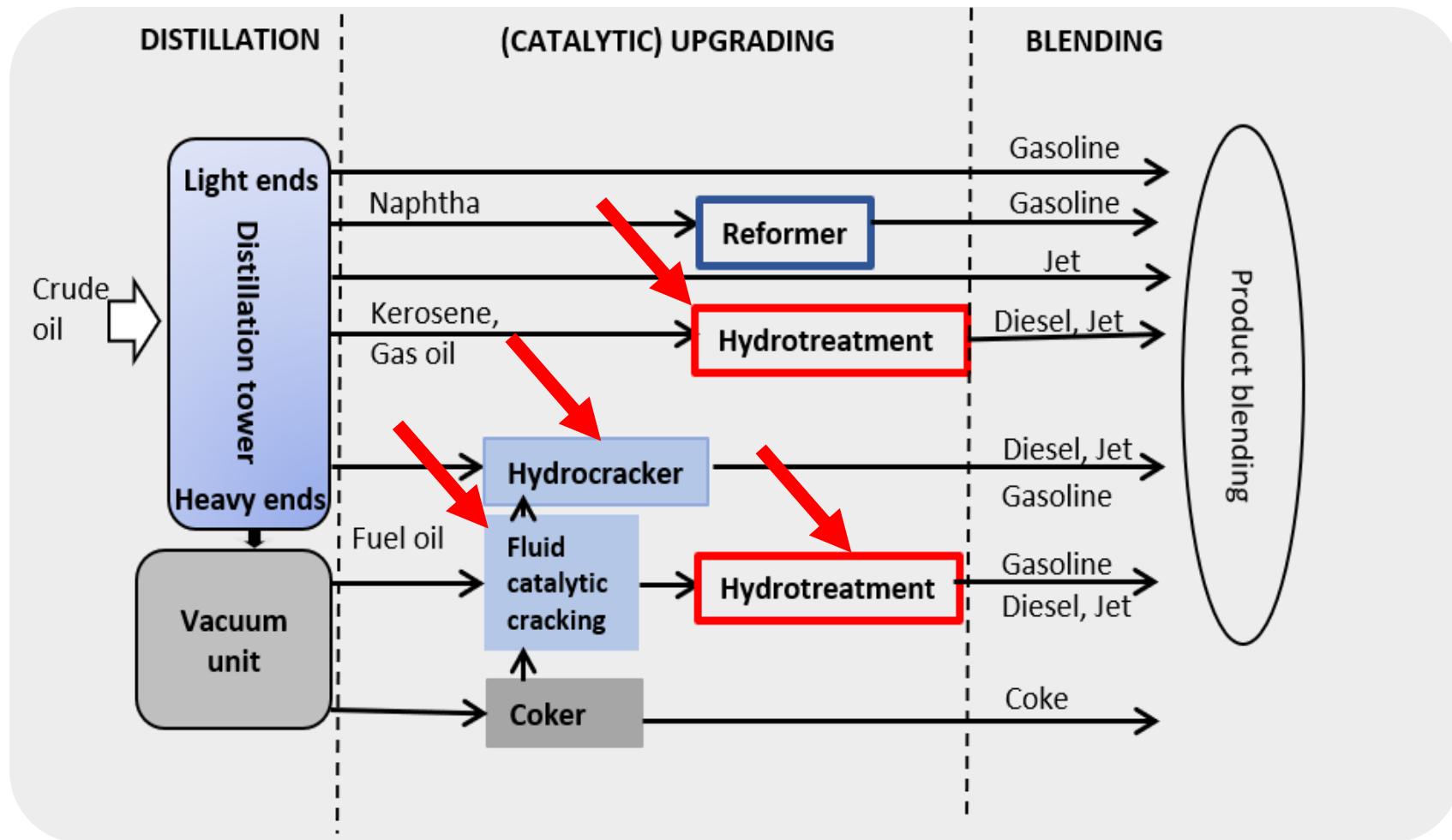
Everywhere in the world, new HVO<sup>1</sup> projects are projected to significantly increase by 2025, triple in the EU, six-fold in the US, and three-fold in Asia compared to 2020



# Co-processing - driven by low carbon fuel standards and favourable policies (SAF)

- Refineries want to lower the CI of their fuels to:
  - Meet LCFS targets
  - Access lucrative markets, e.g., SAF
- Co-processing will become critical for refineries who want to remain relevant in a future net-zero world

# Potential refinery insertion points



# Co-processing feedstocks and upgrading

- Feedstocks for co-processing
  - FOGs, bio-oils/biocrudes, FT Liquids
  - Availability of sufficient feedstock and cost will be key challenges (FOGs)
  - Availability and quality of bio-oils/biocrudes will be challenge
- Where and how you insert depends on:
  - Nature of the feedstock - e.g. is cracking required?
  - Refinery configuration & desired products (gasoline or middle distillates) - likely moving away from gasoline as EVs become more prevalent
  - Potential impact on refinery operations (limitation of risk)

# Refineries engaged in co-processing

- Focus on renewable diesel and SAF
  - Preem - 30% tall oil, moving towards 85%
  - BP Cherry point in Washington State (10+% FOGs in hydrotreater)
  - Parkland Refinery in Burnaby, Canada (10+% FOGs in FCC)
  - BP Castellon refinery in Spain (5% FOGs in hydrotreater for SAF)
  - ENI Taranto Refinery in Italy (5% FOGs in hydrotreater for SAF)
  - Chevron, Exxon, Petrobras, Repsol, Shell, Equinor, Honeywell/UOP



# Challenges of co-processing and technology solutions

- Biobased feedstock characteristics influence coprocessing and present a challenge to the refinery
  - oxygen, TAN, water, alkali metals, lack of miscibility with fossil feeds, high hydrogen consumption, high heat generation, impact on sulfur removal
- Technology solutions developed by several companies (Haldor Topsoe, Shell, Axens, Albermarle, Honeywell/UOP)
  - Optimised pretreatment
  - Modified catalysts to limit inhibition/inactivation
  - Modified reactor configuration to prevent blocking
  - Heat management through quenching
  - Separate injection for immiscible biobased feeds
  - Management of corrosion

# Infrastructure investment to facilitate coprocessing

- At low blends, relatively low costs related to storage, pretreatment, new metallurgy, processing unit modification, new catalyst
- At high blends cost become significant, including increased hydrogen production

# Determining the carbon intensity of co-processed fuels

- Various methods - mass balance, carbon balance, C14 - still under evaluation
- Co-processing of FOGs in the hydrotreater relative simply - similar CI to standalone HVO
- Co-processing in the FCC becomes complicated
  - Companies argue for mass balance allocation using a baseline of the fossil feed alone
  - However, this does not give an accurate measurement
- Work carried out by **Jianping Su at the Parkland Refinery** shows the shortcomings of a mass balance approach

# Challenges in determining the renewable content of the final fuels after co-processing biogenic feedstocks in the fluid catalytic cracker (FCC) of a commercial oil refinery

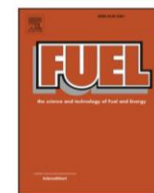
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Full Length Article

Challenges in determining the renewable content of the final fuels after co-processing biogenic feedstocks in the fluid catalytic cracker (FCC) of a commercial oil refinery



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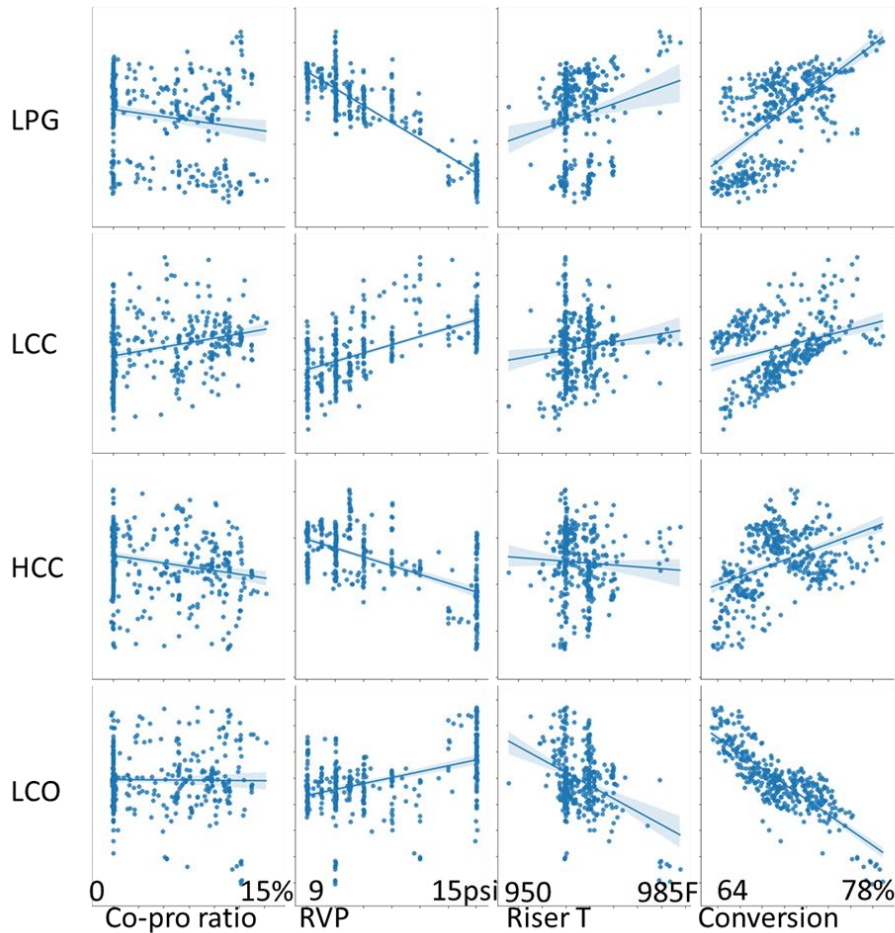
<sup>c</sup> Parkland Refining (B.C.) Ltd., 2025 Willingdon Ave, Burnaby, BC V5J 0J3, Canada

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# Refinery baseline and co-process at low percentage



- Baseline noise is too high for FCC co-processing at low % to generate a strong signal
- Mass balance based on observed yield is problematic (assuming biogenic feed is the only changing variable)
- Long-term data and multiple linear regression used to improve the correlation and quantify the impact of biogenic feedstocks - Plus C14

# Determining the amount of “green” coke when co-processing lipids commercially by fluid catalytic cracking

- Paper has been submitted and passed 1<sup>st</sup> review

**Determining the amount of “green” coke generated when co-processing lipids commercially by fluid catalytic cracking (FCC)**

Jianping Su<sup>a</sup>, Liang Cao<sup>b</sup>, Gary Lee<sup>c</sup>, Bhushan Gopaluni<sup>b</sup>, Don O'Connor<sup>d</sup>, Susan van Dyk<sup>a</sup>, Robert Pinchuk<sup>c</sup>, Jack Saddler<sup>a</sup>

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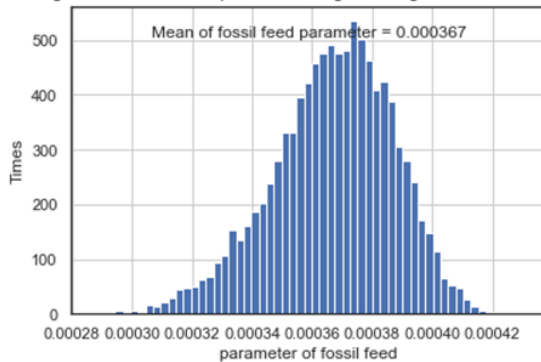
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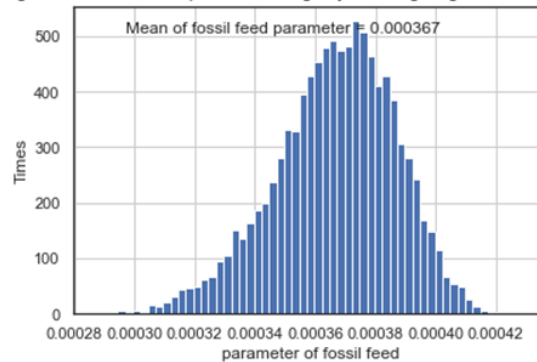
\* Correspondence to: Jack (John) Saddler. E-mail: Jack.Saddler@ubc.ca

# Green coke determination and bootstrap method to reduce the uncertainties

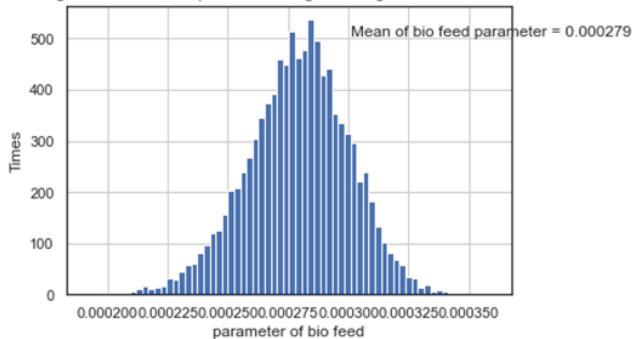
Histogram of the fossil feed parameter using linear regression with all variables



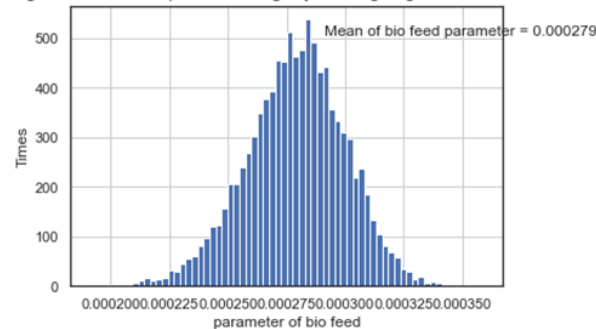
Histogram of the fossil feed parameter using Bayesian ridge regression with all variables



Histogram of the biofeed parameter using linear regression with all variables



Histogram of the bio feed parameter using Bayesian ridge regression with all variables



- FCC co-processing generates green coke
- Can be quantified using a multiple linear regression and use of hourly data
- A bootstrap method can be used to reduce the uncertainties when estimating the coefficients



# Conclusions

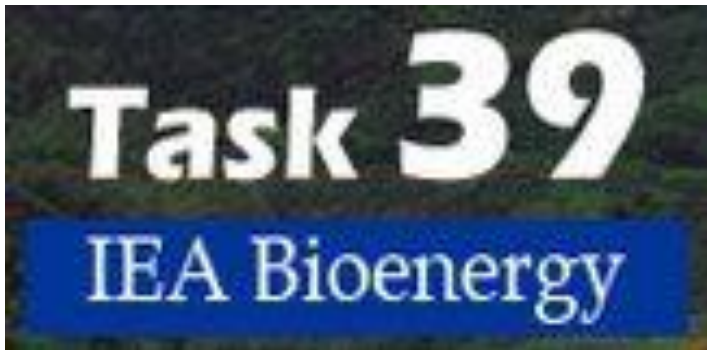
- Stand-alone drop-in biofuel production is rapidly expanding, many HVO, but also other technologies
- Co-processing is increasing due to policies such as LCFS and SAF mandates & incentives, but also part of refinery transformation to a net zero future
- Co-processing of FOGs at commercial level and widespread
- Co-processing of bio-oils/biocrudes still under development due to technical challenges and biocrude availability
- Multiple companies entering the co-processing space and many technologies & catalysts are being developed to overcome technical challenges
- Accurate CI calculation is still challenging



Thank you

Susan van Dyk

Jack Saddler



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